Directed Evolution Reveals Unexpected Epistatic Interactions That Alter Metabolic Regulation and Enable Anaerobic Xylose Use by *Saccharomyces cerevisiae*

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**Abstract**

The inability of native *Saccharomyces cerevisiae* to convert xylose from plant biomass into biofuels remains a major challenge for the production of renewable bioenergy. Despite extensive knowledge of the regulatory networks controlling carbon metabolism in yeast, little is known about how to reprogram *S. cerevisiae* to ferment xylose at rates comparable to glucose. Here we combined genome sequencing, proteomic profiling, and metabolomic analyses to identify and characterize the responsible mutations in a series of evolved strains capable of metabolizing xylose aerobically or anaerobically. We report that rapid xylose conversion by engineered and evolved *S. cerevisiae* strains depends upon epistatic interactions among genes encoding a xylose reductase (*GRE3*), a component of MAP Kinase (MAPK) signaling (*HOG1*), a regulator of Protein Kinase A (PKA) signaling (*IRA2*), and a scaffolding protein for mitochondrial iron-sulfur (Fe-S) cluster biogenesis (*ISU1*). Interestingly, the mutation in *IRA2* only impacted anaerobic xylose consumption and required the loss of *ISU1* function, indicating a previously unknown connection between PKA signaling, Fe-S cluster biogenesis, and anaerobiosis. Proteomic and metabolomic comparisons revealed that the xylose-metabolizing mutant strains exhibit altered metabolic pathways relative to the parental strain when grown in xylose. Further analyses revealed that interacting mutations in *HOG1* and *ISU1* unexpectedly elevated mitochondrial...
respiratory proteins and enabled rapid aerobic respiration of xylose and other non-fermentable carbon substrates. Our findings suggest a surprising connection between Fe-S cluster biogenesis and signaling that facilitates aerobic respiration and anaerobic fermentation of xylose, underscoring how much remains unknown about the eukaryotic signaling systems that regulate carbon metabolism.

Author Summary

The yeast Saccharomyces cerevisiae is being genetically engineered to produce renewable biofuels from sustainable plant material. Efficient biofuel production from plant material requires conversion of the complex suite of sugars found in plant material, including the five-carbon sugar xylose. Because it does not efficiently metabolize xylose, S. cerevisiae has been engineered with a minimal set of genes that should overcome this problem; however, additional genetic changes are required for optimal fermentative conversion of xylose into biofuel. Despite extensive knowledge of the regulatory networks controlling glucose metabolism, less is known about the regulation of xylose metabolism and how to rewire these networks for effective biofuel production. Here we report genetic mutations that enabled the conversion of xylose into bioethanol by a previously ineffective yeast strain. By comparing altered protein and metabolite abundance within yeast cells containing these mutations, we determined that the mutations synergistically alter metabolic pathways to improve the rate of xylose conversion. One change in a gene with well-characterized aerobic mitochondrial functions was found to play an unexpected role in anaerobic conversion of xylose into ethanol. The results of this work will allow others to rapidly generate yeast strains for the conversion of xylose into biofuels and other products.

Introduction

Biofuels, such as ethanol, produced by microbial fermentation of plant-derived feedstocks offer renewable, carbon-neutral forms of energy. Lignocellulosic hydrolysates are generated by chemical pretreatment and hydrolysis of plant cell walls, which are composed of lignin, cellulose, and hemicellulose, and contain glucose, xylose, other carbohydrates, and diverse small molecules. Saccharomyces cerevisiae, the predominant microbe used by the starch ethanol industry, excels at fermenting glucose, but lacks both sufficient metabolic activities and appropriate regulatory responses to ferment xylose rapidly and efficiently [1]. To become economically feasible, microbes must be able to ferment the complete suite of sugars including xylose, which can be up to half of the total fermentable sugar in some lignocellulosic hydrolysates.

In order to achieve a minimal level of xylose catabolism, yeasts have been engineered to express the xylose isomerase (XI)-xylulokinase (XX) pathway or the xylose reductase-xyitol dehydrogenase-xylulokinase pathway to produce xylose-5-phosphate (X5P), which can then be further converted via the pentose phosphate and glycolytic pathways into ethanol (reviewed in [2–5]). Improved xylose-fermenting S. cerevisiae strains were the result of intensive rational engineering to over-express additional metabolic enzymes [6, 7]. Directed evolution has further improved strains to achieve greater fermentative capacity for xylose (reviewed in [1]). However the underlying genetic mechanisms of xylose fermentation remain largely unexplored. To date, three separate studies reported the identities of evolved mutations directly linked to improved
xylose metabolism. These include evolved mutations in the alkaline phosphatase PHO13, which was implicated in xylose catabolism through transposon library screening [8], the hexose transporter HXT7, which caused an increased xylose uptake rate [9], and GRE3 [10], which encodes an aldose reductase that converts xylose into xylitol [11, 12], an inhibitor of xylose isomerase [13]. Even with these genetic modifications, *S. cerevisiae* strains do not achieve industrially acceptable xylose fermentation rates, indicating that additional metabolic and regulatory bottlenecks limit xylose conversion.

In contrast to our limited understanding of xylose metabolism, the regulatory systems that control glucose assimilation in *S. cerevisiae* are among the best-understood networks in eukaryotic cells. Yeast sense and respond to a range of glucose concentrations through multiple signaling pathways that regulate specific transcriptional and metabolic responses. This tight regulatory response to glucose enables *S. cerevisiae* to be one of few organisms that ferment glucose into ethanol aerobically through high glycolytic flux (reviewed in [14]). Three signaling pathways mediated by cyclic AMP (cAMP)-Protein Kinase A (PKA), Snf3/Rgt2, and Snf1 are primarily responsible for coordinating this response (recently reviewed in [15–21]).

Glucose sensing by the G-protein coupled receptor Gpr1p and Ras GTPase activate production of cAMP by adenylate cyclase, which subsequently stimulates PKA activity [22]. Activated PKA has both positive and negative regulatory functions; phosphorylation of cytosolic targets causes activation of glycolysis [23, 24] and other metabolic pathways, whereas phosphorylation of transcription factors causes repression of genes involved in stress response [25] and in the metabolism of non-fermentable carbon substrates [26], such as oxidation of ethanol. Slightly less well understood is the pathway mediated by the paralogous transmembrane sensors Snf3p and Rgt2. Snf3p senses low concentrations of glucose, while Rgt2p acts as a sensor for high glucose concentrations [27, 28]. These sensors fine-tune the expression of a large family of hexose transporters (HXT), which display a range of affinities for binding and transporting glucose according to its extracellular availability. Lastly, the AMP-activated kinase (AMPK) Snf1p is the third rheostat controlling the response to glucose. In the absence of glucose, Snf1p is active and promotes the expression of genes and activation of proteins involved in respiratory metabolism, gluconeogenesis, and the glyoxylate cycle, while repressing anaerobic processes [15, 18]. In the presence of glucose, Snf1p is inactive such that metabolism of ethanol, glycerol, acetate and other non-preferred carbon sources are repressed. Only upon depletion of glucose or other fermentable sugars (e.g., fructose) does *S. cerevisiae* undergo diauxic shift to respire ethanol or other non-fermentable carbon substrates. Through this complex interplay of signaling networks, *S. cerevisiae* is able to achieve rapid conversion of glucose into ethanol.

Despite this extensive understanding of glucose metabolism and numerous research efforts, it remains unclear how to reprogram regulatory networks in *S. cerevisiae* to convert xylose into ethanol or other biofuels rapidly and efficiently. Here, we report novel epistatic genetic interactions between mutations in genes involved in MAPK (*HOG1*) and cAMP-PKA (*IRA2*) signaling pathways, assembly and transfer of Fe-S clusters (*ISU1*) and GRE3 that collectively enable xylose metabolism under various oxygen conditions. Using proteomic and metabolomic analyses, we discovered that loss of *ISU1* function is crucial for aerobic respiration and anaerobic fermentation of xylose, and that epistatic interactions with *IRA2* mutations are essential for anaerobic fermentation. Based on the individual effects of these mutations on protein and metabolite levels and on use of xylose and other carbon sources, we propose a mechanistic model to explain their effects. Our findings have major implications for the understanding of the pathways controlling nutrient signaling and contribute towards improving metabolic engineering for the production of lignocellulosic biofuels.
Results

Mutations in ISU1 and HOG1 underlie aerobic xylose fermentation

Previously, we described the generation and characterization of a series of engineered and sequentially evolved S. cerevisiae strains with a range of abilities to consume and metabolize xylose: (i) GLBRCY22-3 (Y22-3), which was generated from a genetically engineered mono-spore derivative of the stress-tolerant NRRL YB-210 S. cerevisiae strain [29]; (ii) GLBRCY127 (Y127), which is a single clone isolated from the aerobic directed evolution of Y22-3 on xylose; and (iii) GLBRCY128 (Y128), a single clone isolated from the anaerobic directed evolution of Y127 on xylose (Fig 1A and [10]). Here, we set out to define the mutations responsible for improved xylose metabolism at each stage in the evolutionary trajectory, from the parental...
Table 1. Genetic differences between parental and evolved strains.

<table>
<thead>
<tr>
<th>Evolved Strain</th>
<th>Parental Strain</th>
<th>Gene</th>
<th>Functional Gene Annotation</th>
<th>Nucleotide Difference</th>
<th>Amino Acid Difference</th>
</tr>
</thead>
<tbody>
<tr>
<td>Y127</td>
<td>Y22-3</td>
<td>ISU1</td>
<td>Fe-S cluster assembly</td>
<td>C412T</td>
<td>H138Y</td>
</tr>
<tr>
<td>Y127</td>
<td>Y22-3</td>
<td>HOG1</td>
<td>MAP kinase signaling</td>
<td>A844del</td>
<td>M282frame-shift^4</td>
</tr>
<tr>
<td>Y127</td>
<td>Y22-3</td>
<td>GSH1</td>
<td>Glutathione biosynthesis</td>
<td>G839A</td>
<td>R280H</td>
</tr>
<tr>
<td>Y127</td>
<td>Y22-3</td>
<td></td>
<td>Subtelomeric Ty element</td>
<td>A317ins^5</td>
<td>NA</td>
</tr>
<tr>
<td>Y128</td>
<td>Y127</td>
<td>GRE3</td>
<td>Aldose reductase</td>
<td>G136A^6</td>
<td>A46T</td>
</tr>
<tr>
<td>Y128</td>
<td>Y127</td>
<td>IRA2</td>
<td>Inhibitor of RAS</td>
<td>G8782T</td>
<td>E2928Stop</td>
</tr>
<tr>
<td>Y128</td>
<td>Y127</td>
<td>SAP190</td>
<td>Component of St4p phosphatase complex</td>
<td>A2590G</td>
<td>S864G</td>
</tr>
</tbody>
</table>

^1 Saccharomyces Genome Database (http://www.yeastgenome.org/).
^2 Nucleotide and position in parent to evolved mutation.
^3 Amino acid and position in parent to evolved amino acid.
^4 Deletion mutation caused a codon shift in the reading frame.
^5 Insertion of A occurs after nucleotide position 317 in the telomeric region of the left arm of Chromosome XIV.
^6 Published in [10].

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strain Y22-3, to aerobic xylose-consuming Y127, and then to anaerobic xylose-fermenting Y128. To define these mutations, we first mapped Illumina sequence reads from Y127 and Y128 genomes to the sequenced and assembled Y22-3 parental genome [30], and then identified both single nucleotide polymorphisms (SNPs) and DNA insertion/deletion (indel) mutations that arose during the directed evolution (see Materials and Methods). In the Y127 strain, which can rapidly metabolize xylose aerobically, we found non-synonymous SNPs in ISU1 and GSH1, which encode a mitochondrial iron-sulfur (Fe-S) cluster chaperone and γ-glutamylcysteine synthetase, respectively, a single base-pair, frame-shifting deletion in the Mitogen Activated Protein Kinase (MAPK) HOG1, and a single base-pair insertion in a Ty element within the left arm subtelomere of Chromosome XIV (Table 1). The hog1M282fs mutation is predicted to generate a scrambled sequence of 31 amino acids before terminating well short of the 435 amino acids for wild-type Hog1p. Under osmotic and other environmental stresses, Hog1p is phosphorylated by Pbs2p and then translocates into the nucleus to regulate transcription of stress response genes (reviewed in [31]). The mutation iso1H138Y substitution resides adjacent to a functionally important tripeptide domain [32]. ISU1 and its paralog ISU2 encode mitochondrial-localized proteins involved in assembling Fe-S clusters, which are co-factors for proteins involved in electron transfer, enzymatic reactions, and oxygen sensing [33, 34].

During directed evolution, random mutations with neutral or minimal impact on selective growth (so called “hitchhiker” mutations; [35]) can be carried along with beneficial “driver” mutations. Thus, to define the contributions of the hog1, isu1 and gsh1 mutations for aerobic xylose metabolism by Y127, we backcrossed Y127 of opposite mating type to the Y22-3 parent. Forty individual haploid progeny from ten tetrads were then genotyped and phenotyped for their aerobic xylose consumption rates per unit cell mass in comparison to their parental strains. We then compared the genotyped progeny to the Y22-3 and Y127 parent strains (Fig 1B). Progeny containing only the hog1 or gsh1 mutation alone consumed xylose aerobically at similar levels to the non-xylose metabolizing Y22-3 parent, whereas strains harboring only the isu1 mutation consumed xylose albeit at a slower rate compared to the evolved Y127 strain. In contrast, progeny containing both isu1H138Y and hog1M282fs mutations consumed xylose aerobically at significantly faster rates than the isu1H138Yhog1M282fs single mutant and similarly to both the isu1H138Y hog1M282fs gsh1R280H triple mutant progeny and the evolved Y127 parent. We conclude that the mutation in ISU1 was required for the Y127 xylose metabolism phenotype and
its effect was augmented by the \( hog1^{M282fs} \) mutation for the Y127 aerobic xylose metabolism phenotype.

**Additional mutations in GRE3 and IRA2 contribute to anaerobic xylose fermentation**

We next identified the mutations responsible for anaerobic xylose fermentation by the evolved Y128 strain. From sequence comparisons between Y22-3 and Y128, we identified the \( isu1^{H138Y}, hog1^{M282fs}, \) and \( gsh1^{R280H} \) mutations present in Y127 and three additional Y128-specific mutations: (i) the missense mutation in GRE3 reported earlier [10]; (ii) a non-synonymous SNP in IRA2, which encodes a negative regulator of Ras and is an inhibitor of cAMP-PKA signaling [36]; and (iii) a non-synonymous SNP in SAP190, which encodes a component of the Sit4p phosphatase complex [37] and is involved in TOR signaling [38] (Table 1). The mutation in IRA2 causes a nonsense coding change that removes 152 carboxy-terminal amino acids, a region important for Ira2p stability [39]. Loss of IRA2 function is known to activate Ras, subsequently stimulating PKA kinase activity on various target proteins, including trehalose biosynthesis, glycolytic enzymes, and transcription factors controlling ribosomal protein expression and stress response [16]. The missense mutation in SAP190 causes a serine 864 to glycine change. We next crossed the Y128 strain with the Y127 strain of opposite mating type and generated 7 tetrads and 28 haploid progeny, all of which had the \( isu1^{H138Y}, hog1^{M282fs} \) and \( gsh1^{R280H} \) mutations common to both Y127 and Y128. These haploid progeny were then genotyped and phenotyped for their rates of anaerobic xylose consumption per unit cell biomass (Fig 1C) in comparison to Y128 and its predecessor Y127, which does not consume xylose anaerobically. Descendants with either the single \( ira2^{E2928Stop} \) or \( gre3^{A46T} \) mutations, in the context of \( isu1^{H138Y} \) and \( hog1^{M282fs} \) mutations present in Y127, consumed xylose faster than Y127, but slower than Y128. In contrast, double \( ira2^{E2928Stop} gre3^{A46T} \) and triple \( ira2^{E2928Stop} gre3^{A46T} sap190^{A864G} \) mutants (also harboring the Y127 mutations), fermented xylose at rates equivalent to Y128 and significantly faster than \( gre3^{A46T} \) single mutants. Progeny containing the \( sap190^{A864G} \) mutation in combination with an \( ira2^{E2928Stop} \) or \( gre3^{A46T} \) mutation fermented similar amounts of xylose as single \( ira2^{E2928Stop} \) or \( gre3^{A46T} \) mutant strains.

**Mutations in ISU1 and HOG1 interact epistatically for rapid aerobic xylose consumption**

Given that the biological functions of HOG1, ISU1, and IRA2 have not been previously connected to xylose metabolism (Fig 1D), we sought to validate the requirement for the mutations in these genes in xylose metabolism by introducing targeted deletion mutations in a derivative of the Y22-3 parent strain that lacked the \( kanMX \) antibiotic marker used to integrate the XylA-XYL3-TAL1 expression cassette (Y22-3MR, MR, marker-rescued). We first attempted to reconstruct the Y127 aerobic xylose metabolism phenotype by deleting HOG1 and ISU1. Y22-3MR strains harboring various combinations of \( hog1\Delta, ira2\Delta \) and \( gre3\Delta \) mutations were generated and examined for their abilities to grow on and consume xylose aerobically as the sole sugar source (Fig 2A and 2B). We calculated cell growth and specific xylose consumption rates (xylose consumed per unit cell mass), which corrected for differences in xylose consumption due to variation in culture densities, and found that, not surprisingly, the relative differences in growth and consumption rates closely correlated with each other (confirming that growth is dependent upon xylose consumption). The single \( isu1\Delta \) mutant aerobically grew on and consumed xylose faster than the wild-type Y22-3MR parent. In contrast, single-gene deletion of HOG1 had no effect. However, deletion of HOG1 in the context of the \( isu1\Delta \) mutation significantly increased the aerobic growth and xylose consumption rates compared to the \( isu1\Delta \).
Fig 2. Deletions of ISU1, HOG1, GRE3 and IRA2 are sufficient to increase cell growth and xylose consumption rates. Indicated strains were cultured in YPX media under aerobic (A-B) or anaerobic (C-F) conditions. Average growth and specific xylose
consumption rates with standard deviations are reported in g of dry cell mass-hr^{-1} (A, C) or OD600-hr^{-1} (E), and g of xylose consumed g of dry cell mass^{-1}h^{-1} (B, D) or g of xylose consumed OD600^{-1}h^{-1} (F), respectively, from the indicated strains cultured in YP media and YPX media from three independent biological replicates. Asterisks denote statistically significant differences (*, P < 0.05; **, P < 0.061) between specified strains by paired Student’s t-test. Xylose consumption rates for all strains in (D) were significantly faster (P < 0.05) than Y22-3MR.

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mutation alone, with rates equivalent to the Y127 marker-rescued strain (Y127\textsuperscript{MR}), revealing an epistatic interaction between the two mutations. Deletion of \textit{GSH1} alone or in combination with other mutations (S1A and S1B Fig) did not produce statistically significant differences in xylose consumption rates compared to \textit{isu1Δ} and \textit{hog1Δ isu1Δ} strains, confirming that \textit{GSH1} deletion contributed little to the xylose metabolism phenotype. Additionally, strains engineered with deletion mutations in the paralog \textit{isu2} did not consume xylose faster than Y22-3MR (S1C and S1D Fig). Together, these results indicate that synthetic genetic interactions between \textit{hog1Δ} and \textit{isu1Δ} mutations enable rapid aerobic growth on and consumption of xylose.

\textbf{Deletion of IRA2, GRE3, HOG1, and ISU1 enables rapid anaerobic xylose fermentation}

We previously reported that deletion of \textit{GRE3} in the Y127\textsuperscript{MR} \textit{gre3Δ} mutant strain enabled faster anaerobic xylose fermentation than in Y127\textsuperscript{MR} but not at the same rate as Y128\textsuperscript{MR} \cite{10}. Given the identification of the \textit{ira22928Stop} mutation in Y128, we next assessed whether specific deletion of \textit{IRA2} could increase the rate of anaerobic xylose consumption comparable to Y128\textsuperscript{MR}. Indeed, deleting \textit{GRE3} and \textit{IRA2} in the evolved Y127\textsuperscript{MR} and Y128\textsuperscript{MR} genetic backgrounds enabled cells to consume and grow on xylose anaerobically at rates equivalent to Y128\textsuperscript{MR} (S2A and S2B Fig). Additional deletion of \textit{SAP190} had no effect in the Y127\textsuperscript{MR} \textit{gre3Δ} \textit{ira2Δ} background but impaired xylose consumption and growth in the Y128\textsuperscript{MR} \textit{gre3Δ} \textit{ira2Δ} background (S2A and S2B Fig). Interestingly, deletion of the \textit{IRA2} paralog, \textit{IRA1}, in the Y127\textsuperscript{MR} \textit{gre3Δ} background yielded a strain with intermediate rates of anaerobic xylose consumption and growth compared to Y127\textsuperscript{MR} \textit{gre3Δ} and Y127\textsuperscript{MR} \textit{gre3Δ} \textit{ira2Δ} mutants (S2C and S2D Fig). We conclude that loss-of-function mutations in \textit{IRA2} contribute to anaerobic xylose consumption and that alternative loss of \textit{IRA1} function can also facilitate moderate anaerobic xylose fermentation, indicating that Ira2p and Ira1p are not entirely redundant for function. These observations could reflect differences in either activities or expression levels.

As a further test for the role of \textit{ira2} and \textit{gre3} mutations in anaerobic xylose fermentation, we determined the cell growth, specific xylose consumption and ethanol production rates of Y22-3\textsuperscript{MR} strains engineered with various combinations of deletions in flasks (Fig 2C and 2D, S3A Fig) and in controlled bioreactors sparged continuously with N\textsubscript{2 }gas (S4 Fig). Deletion of \textit{IRA2} or \textit{GRE3} increased the growth, specific anaerobic xylose consumption, and ethanol production rates in the context of the \textit{hog1Δ isu1Δ} double knockout. Moreover, simultaneous deletion of \textit{HOG1, ISU1, IRA2, and GRE3} resulted in specific xylose consumption and ethanol production rates comparable to Y128\textsuperscript{MR}. Interestingly, double deletion of \textit{GRE3} and \textit{IRA2} alone had limited impacts on aerobic (Fig 2A and 2B) or anaerobic (Fig 2C and 2D, S3A and S4 Figs) xylose consumption, ethanol production and growth relative to the Y22-3\textsuperscript{MR} parent, suggesting that loss-of-function \textit{hog1} and \textit{isu1} mutations were crucial for enabling anaerobic xylose fermentation. Indeed, we found that deletions of \textit{ISU1, GRE3, and IRA2} together conferred anaerobic growth, consumption, and ethanol production on xylose nearly equivalent to deletion of all four genes (Fig 2E and 2F, S3B Fig), but deletions of \textit{HOG1, GRE3, and IRA2} had a minimal effect. Together, these results indicate that loss of \textit{ISU1} function is a major contributor to anaerobic conversion of xylose.
To determine the generality of the effects caused by mutations in these newly-implicated pathways, we engineered xylose catabolism into two different, commonly used laboratory yeast strains: BY4741 [40], which was derived from S288c, and CEN.PK113-5D [41], a derivative of CEN.PK2 that is often engineered for xylose metabolism studies [42]. BY4741 and CEN. PK113-5D strains were engineered with the same DNA cassette that allowed expression of bacterial xylose isomerase, fungal XYL3 and yeast TAL1 [10] in the Y22-3<sup>MR</sup> strain. Subsequent deletions of HOG1, ISU1, GRE3, and IRA2 were sufficient to confer significantly faster anaerobic consumption of xylose in both BY4741 and CEN.PK113-5D backgrounds (S5B Fig), and significantly faster cell growth and ethanol production in the CEN.PK113-5D background (S5A and S5C Fig). Thus, the combined abilities of the hog<sup>1</sup>Δ, isu<sup>1</sup>Δ, gre<sup>3</sup>Δ, and ira<sup>2</sup>Δ mutations to confer anaerobic conversion of xylose into ethanol are not limited to the Y22-3<sup>MR</sup> strain background.

Mutations enabling xylose metabolism also affect metabolism of other carbon substrates

Although we carried out directed evolution specifically on xylose, the roles of Hog1p, Isu1p, and Ira2p in biochemical pathways of broad function raised the possibility that these evolved mutations could impact carbon metabolism more generally. We tested this possibility by measuring the growth and consumption rates of various deletion strains on a variety of carbon sources, which are consumed through different entry points of central metabolism compared to xylose (S6A Fig). For glucose, the mutations had minimal effects on aerobic growth and consumption rates (Fig 3A and 3B). In contrast, we found that hog<sup>1</sup>Δ isu<sup>1</sup>Δ mutants grew on and consumed glycerol (Fig 3C and 3D) and acetate (Fig 3E and 3F) significantly faster than the parental Y22-3<sup>MR</sup> strain under aerobic conditions. On the other hand, hog<sup>1</sup>Δ and isu<sup>1</sup>Δ single mutations caused modest or no increases in galactose (S6B and S6C Fig) and ethanol (S6D and S6E Fig) growth and consumption rates. Unlike the effect of isu<sup>1</sup>Δ on xylose consumption, deletion of ISU1 did not improve the consumption rates of these other carbon substrates significantly. Rather, deletion of HOG1 alone, which had no effect on aerobic xylose metabolism, resulted in significantly faster glycerol and acetate consumption rates with slight to no effect on growth rates. Quadruple deletions of HOG1, ISU1, GRE3 and IRA2 did not significantly alter anaerobic growth or glucose consumption rates (Fig 3G and 3H), but produced significantly faster growth on and consumption of galactose anaerobically than other combinations of the mutations (S6F and S6G Fig). This suggests that the combined mutations enabling xylose metabolism also confer more rapid consumption of non-preferred carbon substrates, but that the genetic architectures and epistatic interactions vary for each carbon source.

Proteomic analysis revealed altered abundance of proteins involved in metabolism and stress response

To shed light on the molecular mechanisms by which the mutations in HOG1, ISU1, and IRA2 increased the rate of xylose metabolism by yeast, we compared the protein abundances of the various strains normalized to the proteome of the parental Y22-3<sup>MR</sup> strain cultured in xylose aerobically and anaerobically. We identified proteins and enriched functional groups whose abundances were significantly different across strains by statistical (False discovery rate, FDR <0.05, S7A Fig, S3 and S4 Appendixes) and clustering (Fig 4) analyses. We first compared proteome differences in Y127<sup>MR</sup> and the parental Y22-3<sup>MR</sup> strains grown aerobically on xylose as the sole carbon source (S3 and S4 Appendixes); over 800 proteins showed statistically significant abundance differences across the two strains. Proteins at lower abundance in the evolved Y127<sup>MR</sup> strain versus the parental Y22-3<sup>MR</sup> strain were enriched for proteins involved
Epistatic Genetic Interactions Enable Xylose Metabolism in Evolved Yeast

A

![Graph A: Growth Rate vs. HOG1 ISU1, hog1Δ, isu1Δ, hog1Δ isu1Δ in YPD + O2](image)

B

![Graph B: Specific Glucose Consumption Rate vs. HOG1 ISU1, hog1Δ, isu1Δ, hog1Δ isu1Δ in YPD + O2](image)

C

![Graph C: Growth Rate vs. HOG1 ISU1, hog1Δ, isu1Δ, hog1Δ isu1Δ in YP-Gly + O2](image)

D

![Graph D: Specific Glucose Consumption Rate vs. HOG1 ISU1, hog1Δ, isu1Δ, hog1Δ isu1Δ in YP-Gly + O2](image)

E

![Graph E: Growth Rate vs. HOG1 ISU1, hog1Δ, isu1Δ, hog1Δ isu1Δ in YP-Acetate + O2](image)

F

![Graph F: Specific Acetate Consumption Rate vs. HOG1 ISU1, hog1Δ, isu1Δ, hog1Δ isu1Δ in YP-Acetate + O2](image)

G

![Graph G: Growth Rate vs. HOG1 ISU1, hog1Δ, isu1Δ, hog1Δ isu1Δ, gre3Δ ira2Δ, hog1Δ isu1Δ gre3Δ ira2Δ in YPD - O2](image)

H

![Graph H: Specific Glucose Consumption Rate vs. HOG1 ISU1, hog1Δ, isu1Δ, gre3Δ ira2Δ, hog1Δ isu1Δ gre3Δ ira2Δ in YPD - O2](image)
in alternative energy usage, stress defense, including proteins linked to alternative carbon metabolism, ethanol catabolism, fatty acid ω-oxidation, the pentose phosphate shunt, and proteins in the environmental stress response (ESR, [43], Fig 4, Clusters B and C). These differences are consistent with a starvation response in Y22-3MR strain and that has been alleviated in the evolved Y127MR strain. Altered starvation responses have been linked to differences in growth rate [44–46], which could also impact their relative abundances in Y127MR versus Y22-3MR strains (see below for additional discussion). Additionally, Y127MR displayed higher abundance of approximately 72% of 1,208 mitochondrial proteins reported elsewhere ([47], Fig 4, Clusters D and E). The proteins in these clusters included those linked to mitochondrial transport, translation, and respiration, as well as proteins involved in lipid biogenesis and Golgi and ER functions (S7A Fig). Deletion of ISU1 alone, which caused an intermediate enhancement in xylose consumption rate, recapitulated many of the proteomic differences seen in Y127MR, including increased abundance of mitochondrial proteins (Fig 4, Cluster D and E) that may have enabled faster xylose consumption rates. In contrast, deletion of HOG1 alone caused minor differences in protein abundances compared to Y22-3MR. Interestingly, deletion of HOG1 in the context of the ISU1 deletion did not significantly alter mitochondrial protein abundances relative to the isu1Δ mutant. This strongly suggests that the increased abundances of mitochondrial proteins in Fig 4, Clusters D and E were responses to the isu1 mutations.

We next compared the proteomes of strains with varying abilities to ferment xylose anaerobically (Fig 4, S7B Fig, S3 and S5 Appendices). Both Y128MR and quadruple deletion mutants displayed signatures of elevated PKA signaling compared to Y127MR and hog1Δisu1Δ double mutants, including lower abundance of proteins linked to stress defense and trehalose biogenesis (Fig 4, Cluster B), and higher abundances of proteins involved in glycolysis (Fig 4, Cluster D) and ribosome biogenesis (Fig 4, Cluster E). Indeed, many of the mRNA targets in these clusters are regulated by the phosphodiesterase Pde2, which also inhibits PKA signaling similar to Ira2, as well as Hog1, in response to salt stress [48]. Strains containing ira2Δ or ira2Δ2928Stop mutations specifically displayed both lower expression of trehalose biosynthesis enzymes and intracellular trehalose levels (S8 Fig), which have been observed elsewhere [49, 50]. Unexpectedly, isu1Δ and ira2ΔH138F mutant strains also contained lower intracellular trehalose under aerobic conditions (S8D Fig). Some of these proteomic changes could be simply a secondary response from strains capable of growing on xylose versus Y22-3MR, which cannot. However, at least some are likely to be a direct regulatory response to the mutations. For example, deletion of IRA2 produced many of the growth-related signatures (i.e., lower abundance of stress proteins and higher abundance of many proteins related to ribosome biogenesis), even though this strain cannot grow on xylose without additional mutations (see Fig 2A). This result shows that regulation of the growth-correlated signature is a direct response of PKA signaling, which can be decoupled from growth. Unlike the other mutations, deletion of GRE3 did not produce major proteome changes even though it significantly enhanced xylose fermentation and cellular growth rate on xylose. This suggests that the main contribution of gre3 mutations is to minimize xylitol production, and further indicates that differences in growth rate cannot explain the proteome differences we observe in these conditions.
Epistatic Genetic Interactions Enable Xylose Metabolism in Evolved Yeast
Xylose-metabolizing strains exhibited altered pentose phosphate pathway activities compared to non-xylose metabolizing strains

Based on the proteome-scale signatures, we focused further comparative analyses on proteins and metabolites directly involved in xylose metabolism. Catabolism of xylose to ethanol in Y22-3MR and evolved strains occurs by assimilation of xylose via native hexose transporters Gal2p, Hxt4p, Hxt5p and Hxt6/7p [51], xylose conversion to xylulose-5-phosphate, which is then metabolized through the non-oxidative pentose phosphate and glycolytic pathways into ethanol anaerobically or respired aerobically (Fig 5A). As expected, Y128Δ and strains containing gre3Δ mutations expressed very low or undetectable levels of Gre3p peptides relative to Y22-3MR, suggesting that the gre3A467T mutation may destabilize the protein (Fig 5B and 5C). Strains with mutations in HOG1 also had lower abundances of Gre3p compared to Y22-3MR, which is consistent with a report that Hog1p regulates GRE3 expression [52]. Interestingly, under both aerobic and anaerobic conditions, we observed relatively low or undetectable levels of Tkl2p in Y127Δ and isu1A strains; Tkl2p is one of two trans-ketolases functioning in the pentose phosphate pathway. We also observed low levels of Nqm1p, a paralog of transaldolase Tal1p with unknown function, in all xylose-metabolizing strains relative to the Y22-3MR parent. The metabolomic profile of the same strains indicated that both aerobic and anaerobic xylose-fermenting strains accumulated more pentose phosphate intermediates than Y22-3MR (xylulose-5-phosphate, ribulose-5-phosphate, ribose-5-phosphate and sedoheptulose-7-phosphates; Fig 5D and 5E). These patterns suggest that the combinations of enabling mutations in Y127 and Y128 overcame several of the initial bottlenecks in import and conversion of xylose into xylulose-5-phosphate and thereby uncovered downstream bottlenecks in the pentose phosphate pathway and beyond, increasing the levels of pentose phosphate intermediates. In contrast, there was no strong correlation between TCA cycle enzyme abundance and strain phenotypes aerobically or anaerobically (S9 Fig), although significant changes in TCA cycle metabolites appeared in aerobic xylose metabolizing strains. Specifically, aerobic xylose-metabolizing strains accumulated higher levels of succinate and lower levels of citrate, aconitate, isocitrate, and malate relative to non-xylose metabolizing strains (S9D and S9E Fig). However, these differences could be due to the fact that these metabolites are shared with the glyoxylate cycle (see below).

isu1Δ mutation has essential aerobic and anaerobic functions in xylose metabolism

Pair-wise proteomic comparisons between strains with isu1Δ or isu1H138Y mutations to strains with wild-type ISU1 identified increased abundance of proteins functioning in mitochondrial protein translation and respiration, and decreased abundance of glucose repressed proteins under aerobic conditions (Fig 4 and S7A Fig). We next directly compared the abundances of proteins involved in mitochondrial translation, coenzyme Q biosynthesis [53] and cytochrome c oxidase subunits [54] in all strains according to their abilities to grow on and metabolize
Epistatic Genetic Interactions Enable Xylose Metabolism in Evolved Yeast

A

D-Xylose → Gre3p → D-Xylose → ATP
XylA → Xylose Catabolism
D-Xylose → Xyl3p → Xyl1p → ATP

Ribulose-5P → X-5P → Ribose-5P

E-4P → F-6P → F-1,6-BP

Glycolysis

Tpi1 → GA-3P → DHAP

Non-Oxidative Pentose Phosphate Pathway

Acetyl-CoA → Respiration

Ethanol → Fermentation

B

Non-Xylose Metabolizing Strains

Aerobic Xylose Metabolizing Strains

C

Non-Xylose Fermenting Strains

Anaerobic Xylose Fermenting Strains

D

Non-Xylose Metabolizing Strains

Aerobic Xylose Metabolizing Strains

E

Non-Xylose Fermenting Strains

Anaerobic Xylose Fermenting Strains

PLOS Genetics | DOI:10.1371/journal.pgen.1006372 October 14, 2016 14 / 31
Fig 5. Xylose-metabolizing strains have altered pentose phosphate pathways. Heat maps display intracellular concentrations of proteins and metabolites from xylose metabolism, pentose phosphate pathway and glycolysis (A) from engineered and evolved strains relative to Y22-3Δ. Colors correspond to average Log2 fold change values from strains cultured under aerobic (B and D) or anaerobic (C and E) conditions in YPX medium from three biological replicates. White boxes indicate strains for which no corresponding peptides were detected. The asterisk (*) in (A) denotes an enzyme activity that is absent in the Y22-3Δ strain. Abbreviations: X-5P, xylose-5-phosphate; S-7P, sedoheptulose-7-phosphate; F-6P, fructose-6-phosphate; F-1,6-BP, fructose-1,6-bisphosphate; DHAP, dihydroxyacetone-phosphate; 3- and 2-PG, 3- and 2-phosphoglycerates; PEP, phosphoenolpyruvate.

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xylose aerobically (Fig 6A). Noticeably, most of these proteins were expressed at higher abundances in all five xylose-metabolizing strains with the isu1Δ or isu1ΔH138Y mutations compared to strains with wild-type ISU1. Conversely, glucose-repressed proteins involved in the metabolism of non-fermentable carbon substrates (e.g., glycerol, ethanol, and acetate), in the glyoxylate cycle, in gluconeogenesis, and in fatty acid β-oxidation were expressed at lower abundances in aerobic xylose-metabolizing strains compared to non-xylose metabolizing strains (Fig 6B). Interestingly, yeast lacking the Yeast Frataxin Homologue 1 (YFH1), which functions together with Isu1p in Fe-S cluster assembly, down regulated expression of the same glucose-repressed genes when grown on glycerol [55]. The hexose transporter Hxt5p, which is induced in the presence of non-fermentable carbon sources [56], was similarly detected at lower levels in xylose-metabolizing strains. These results also indicated that altered succinate, citrate, aconitate, isocitrate, and malate levels between strains likely reflected changes in the concentrations of glyoxylate cycle intermediates (S9B Fig). Similar proteomic differences among xylose-fermenting and non-fermenting strains were not seen under anaerobic conditions (S10 Fig), indicating that these effects were specific to aerobic conditions. These proteomic patterns suggest that strains containing isu1Δ or isu1ΔH138Y mutations were not starved on xylose aerobically and did not activate pathways that scavenge non-fermentable carbon sources from the medium, whereas strains with wild-type ISU1 equated the presence of xylose as the sole carbon source to glucose depletion.

The capacity to respire xylose could explain the emergence of the isu1ΔH138Y mutation in Y127 during the directed evolution of Y22-3 on xylose aerobically. To determine whether xylose was respired under aerobic conditions, we treated hog1Δ isu1Δ mutant cells grown with Antimycin A, an inhibitor of oxidative phosphorylation [57]. As expected, the addition of Antimycin A to medium containing ethanol, which can only be respired, blocked cell growth and ethanol consumption one h after treatment, whereas the DMSO only-treated culture continued to grow on and consume ethanol (Fig 6C). We next treated the same yeast strain cultured aerobically on glucose, which can be fermented into ethanol in the presence of oxygen. In contrast, the hog1Δ isu1Δ mutant strain continued to grow on and ferment glucose into ethanol up to 2 h after Antimycin A treatment (Fig 6D), indicating that Antimycin A did not affect fermentative growth and metabolism. Once all of the glucose was consumed by 8 h, the culture grew from respiration of ethanol with DMSO treatment but not with Antimycin A. Treatment with Antimycin A, but not with DMSO, profoundly blocked aerobic growth on and consumption of xylose similar to what was seen for ethanol (Fig 6E). Together, these results indicate that loss of function mutations in ISU1 and HOG1 enabled growth on and catabolism of xylose through respiration. This result was surprising given that the isu1Δ mutations are required for anaerobic xylose fermentation, revealing an oxygen-independent role for ISU1 mutations in driving xylose metabolism.

Discussion

Through combined genome sequence comparisons and genetic approaches, we identified novel epistatic genetic interactions between mutations in HOG1, ISU1, GRE3, and IRA2 that
enabled anaerobic xylose fermentation across multiple yeast strains engineered with xylose isomerase. Mutations in \textit{GRE3} and \textit{IRA2} were only beneficial for anaerobic xylose fermentation and required additional mutations in \textit{HOG1} and \textit{ISU1} to fully recapitulate the evolved Y128 phenotype (Fig 2C and 2D). Based on our combined genetic, proteomic, and metabolomic studies, we propose a model by which the mutations in the evolved Y127 and Y128 strains emerged and enabled xylose metabolism (Fig 7). The parental Y22-3 strain lacks sufficient metabolic activities in one or more steps in xylose catabolism, the pentose phosphate pathway, the glycolytic pathway, or some combination, to permit significant growth and fermentation of xylose aerobically or anaerobically (Fig 7A). Due to this inability, Y22-3 and other non-xylose

Fig 6. Mutations in \textit{ISU1} enhance respiration of xylose. Engineered and evolved strains were cultured in aerobic YPX media and analyzed for intracellular protein and metabolite concentrations. Average Log2 intracellular concentrations of mitochondrial translation and respiration proteins (A) or hexose transporters and glucose-repressed proteins (B) from mutant strains relative to the Y22-3MR parent are shown. White boxes indicate strains for which no corresponding peptides were detected. Relative protein concentrations were calculated from three independent biological replicates. Y22-3MR, hog1Δ, and isu1Δ strains were cultured in YP-Ethanol (C), YPD (D) or YPX (E) media and then treated with DMSO control or 0.5 μg/mL Antimycin A. Shaded areas represent the time during which DMSO or Antimycin A were present in the cultures. Average cell density, sugar and ethanol concentration with standard deviations from three independent biological replicates are reported.

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Epistatic Genetic Interactions Enable Xylose Metabolism in Evolved Yeast

A

Epistatic Genetic Interactions Enable Xylose Metabolism in Evolved Yeast

Y22-3
YPX +/- O_2

Xylose
→
Xylose Catabolism
→
Upper Glycolysis
→
PPP
→
Lower Glycolysis
→
Fermentation, Ethanol Production
→
Respiration, Cell Growth

B

Epistatic Genetic Interactions Enable Xylose Metabolism in Evolved Yeast

Y127
YPX + O_2

Xylose
→
Xylose Catabolism
→
Upper Glycolysis
→
PPP
→
Lower Glycolysis
→
Fermentation, Ethanol Production
→
Respiration, Cell Growth

C

Epistatic Genetic Interactions Enable Xylose Metabolism in Evolved Yeast

Y128
YPX - O_2

Xylose
→
Xylose Catabolism
→
Upper Glycolysis
→
PPP
→
Lower Glycolysis
→
Fermentation, Ethanol Production
→
Respiration, Cell Growth
metabolizing strains under aerobic conditions experience starvation stress, and respond by activating the ESR and Snf1p-controlled pathways that ordinarily allow metabolism of non-preferred and non-fermentable carbon substrates using the glyoxylate cycle (Figs 4 and 6B). Other transcriptomic and metabolomic studies of xylose metabolism identified up-regulation of glyoxylate cycle and non-fermentable carbon metabolism genes [58–62]; however, in some cases, these data were interpreted as an indication that up-regulation of these pathways was needed for xylose metabolism.

Despite the inability of Y22–3 to metabolize xylose, the power of aerobic selective pressure drove the emergence of the Y127 strain. The acquisition of mutations in HOG1 and ISU1 permitted the Y127 strain to overcome a number of biochemical bottlenecks for aerobic xylose metabolism (Fig 7B), possibly through altered xylose catabolism and pentose phosphate pathway activities (Fig 5B and 5D). Loss of ISU1 function also enhanced aerobic respiration of xylose, as suggested by up-regulation of respiratory proteins in isu1 mutants (Fig 6A) and the complete block in aerobic xylose consumption by Antimycin A (Fig 6C–6E). Previous studies indicate that mitochondrial protein translation and oxidative phosphorylation are tightly co-regulated (reviewed in [63]). Specifically, Fe-containing heme is involved in both translation and assembly of cytochrome c oxidase (COX) subunits into the final enzymatic complex of the mitochondrial respiration chain [64, 65]. Thus, loss of ISU1 function may have impaired Fe-S cluster formation and increased the availability of Fe for heme biosynthesis. This could promote the formation of active COX complexes to enhance respiration of xylose and other carbon substrates (Figs 2 and 3, S6 Fig). Alternatively, loss of ISU1 function may have caused an expansion in mitochondrial mass to compensate for the reduced capacity to generate Fe-S clusters. Either case could cause increased abundances of mitochondrial proteins in isu1 mutants (Figs 4 and 6A) and subsequently result in faster xylose respiration. However, the isu1 mutations were also required for anaerobic xylose growth, which involves fermentation and part of glycolysis but not respiration; thus, the role of isu1 mutations in anaerobic xylose use is unclear and will require further investigation.

The mechanistic explanation for the emergence of mutations in HOG1 may be related to its suppression of metabolism and growth during stress through phosphorylation of transcriptional regulators or cytosolic factors. First, we (Fig 5B and 5C) and others [12] found that Hog1p positively regulates the expression of GRE3. Thus, the lowered expression of Gre3p in HOG1 mutants reduced the production of inhibitory xylitol and permitted faster xylose catabolism. Additionally, both limited glucose availability [66] and non-fermentable carbon substrates [67] were found to activate Hog1p. Snf1p, which is essential for metabolism of non-preferred carbon sources, also plays a critical role in regulating Hog1p activity under endoplasmic reticulum and starvation stress [67, 68]. The role of Hog1 activation under these conditions was thought to decrease production of cellular biomass, perhaps to balance growth demand with energy availability. Although it is certainly possible that Hog1 mediates transcriptional responses that normally inhibit xylose metabolism, Hog1-mediated phosphorylation of
metabolic enzymes, such as GAPDH/Tdh3 [69], may also limit xylose utilization. Thus, we propose that deletion of HOG1 relieves growth inhibition and restores glycolytic activity in response to non-glucose carbon sources. With enhanced respiration providing greater energy yield from xylose with isi1 mutations, the additional mutations in HOG1 subsequently allow for uninhibited aerobic growth on xylose.

The specific impacts of mutations in GRE3 and IRA2 in enabling anaerobic xylose metabolism, as well as their epistatic interactions with hog1 and isi1 mutations, were unexpected (Fig 7C). Gre3p is a known inhibitor of xylose isomerase through its production of xylitol from xylose, and deletion of GRE3 is known to improve xylose metabolism [10, 13]. Nevertheless, the emergence of the gre3A46T mutation during anaerobic evolution on xylose is notable, indicating that reduced GRE3 expression from the hog1M282fs mutation during aerobic evolution was insufficient. The cAMP-PKA pathway is a well-known positive regulator of sugar metabolism and cellular growth (reviewed in [16, 20, 70]); PKA phosphorylates and positively regulates the activities of key glycolytic enzymes, including pyruvate kinase (Cdc19 and Pyk2), for glucose fermentation. Thus, activation of PKA from the inactivating E2928 to stop mutation in IRA2 may enhance glycolytic flux under anaerobiosis, resulting in faster conversion of xylose into ethanol (Fig 7C). Although other experimental evolution studies also uncovered mutations in IRA that provided fitness advantages under aerobic glucose limitation [35, 71], our studies identified a novel, anaerobic-specific function for PKA signaling since ira2 mutations have little effect on aerobic xylose metabolism (Fig 2C and 2D), and unexpectedly require mutations in ISU1 for anaerobic xylose consumption (Fig 2E and 2F). To date, a direct anaerobic function for ISU1 has not been identified. Together, epistatic genetic interactions between the hog1M282fs, isi1H138Y, gre3A46T and ira2E2928Sop mutations enhance the rate of anaerobic xylose fermentation through the pentose phosphate and glycolytic pathways.

The conversion of xylose into ethanol by yeast is a major bottleneck in lignocellulosic biofuel production [2, 4]. Efficient and rapid xylose fermentation is necessary for cost effective production of biofuels. A number of studies have genetically engineered S. cerevisiae for xylose metabolism, including targeted overexpression of pentose phosphate pathway enzymes, as well as the deletion of GRE3, PHO13 and genes involved side product pathways [2, 7, 8, 72, 73]. To date, only one study has employed genome sequence comparisons to identify candidate sequence differences involved in evolved xylose metabolism phenotypes [8], which subsequently identified a mutation in PHO13. Our genetic and multiomic studies provide the first direct evidence that loss of function mutations in HOG1, ISU1, GRE3, and IRA2 enable xylose fermentation through altered xylose catabolism, pentose phosphate pathway, glycolysis and respiration, and provide an advance in the identification of new genetic targets and pathways for improving xylose metabolism. Nonetheless, challenges remain in developing yeast strains capable of fermenting xylose from lignocellulosic hydrolysates, which are well known to contain microbial inhibitors and toxins that impact yeast xylose fermentation and induce stress responses [74–77]. This is particularly true for strains containing loss of HOG1 function [31] or an activated cAMP/PKA pathway [25], both of which are known to result in reduced stress tolerance. Future studies will be aimed at defining specific genes and pathways that enable rapid and efficient conversion of xylose into biofuels in the presence of these lignocellulose-derived inhibitors.

Materials and Methods

Media

Standard undefined yeast lab medium was prepared as previous described [78]. Briefly, liquid and plate-based medium contained 10 g/L yeast extract and 20 g/L peptone (YP), and various
sugar concentrations (X = 20–30 g/L xylose, D = 20 g/L dextrose/glucose, Gal = 20 g/L galactose, Gly = 20 g/L glycerol, EtOH = 15 g/L ethanol, Acetate = 20 g/L acetate). For anaerobic bioreactor experiments, YPX media also contained 50 mM potassium phosphate, pH 5.5.

**Yeast strains**

Yeast strains used in this study are described in S1 Table. Generation of Y22-3, Y127 and Y128 strains is described elsewhere [10]. The Y174 and Y176 strains were constructed in an identical manner to Y22-3 by integrating the ScTAL1-CpxylA-ScXYL3-loxP-kanMX-loxP cassette into the HO locus of BY4741 [40] and CEN.PK113-5D [79], respectively, followed by excision of the kanMX marker by Cre recombinase [80]. The Y127 MATα strain (GLBRCY156) was generated by diploidization of Y127 [81], sporulation, tetrad dissection and mating type identification [78]. For backcrossing, Y22-3 or Y128 was mated to Y156, subjected to sporulation and tetrad dissection. All tetrad spores were verified for 2:2 segregation of mating type. Diploid spores from 10 sets of Y22-3 X Y157 tetrads were generated, from which the hogM2826, isuI138, gshH3260H, and gshH3260H mutations segregated 2:2 in all progeny. Similarly, haploid spores from 7 sets of Y157 X Y128 tetrads were generated, from which gre3A467, ira2E29825Stop, and sap190S864G mutations segregated 2:2 in all progeny. Deletion of GRE3, ISU1, ISU2, IRA1, IRA2, GSH1 and SAP190 were performed by integration of polymerase chain reaction (PCR) product generated from LoxP-kanMX-LoxP or LoxP-hphMX-LoxP plasmid templates [10, 80] and primers containing 40–60 bp of homology flanking the targeted gene. For deletion of HOG1, gDNA from a hog1Δ::kanMX4 mutant strain [82] was used as the PCR template. PCR products were purified and transformed [83] into the appropriate strains. Cre recombinase-mediated excision of LoxP-flanked antibiotic markers was carried out as published elsewhere [80]. All strains were confirmed for gene deletion and antibiotic marker excision by PCR with independent outside flanking primers. Sanger sequencing of PCR products and DNA plasmids was performed by the University of Wisconsin-Madison Biotechnology Center.

**Genomic DNA sequence comparisons**

For identification of genome sequence differences between strains, including single nucleotide polymorphisms (SNPs) and indels, 100 bp paired end Illumina short reads from Y127 and Y128 genomic DNA were generated as previously described [30]. First, paired-end reads were mapped to either the reference genome Y22-3 [30] or a variant of the S288c reference genome (NC_001133, version 64, [84]) in which the Y22-3 alleles identified by GATK [85] were replaced using Bowtie2 [86] with default settings. Y127 and Y128 SNPs and indels were further identified with GATK using base quality score recalibration, indel realignment and duplicate removal. Default parameters were used except -mbq 25 to reduce false-positive variant calls. Variants were then filtered using the following suggested GATK criteria: QD < 2, FS > 60, MQ < 40. The identified variants were substituted into the S288c reference genome, and to this 100-bp paired end reads from the evolved strains were mapped, followed by GATK analysis as above to define mutations in the evolved strains. Mutations were also identified using similar parameters by mapping to the assembled Y22-3 genome [30]. Non-synonymous mutations in each strain were verified by genomic DNA extraction (Masterpure Yeast DNA Purification Kit, Epicentre), PCR with gene-specific primers (Phuslon DNA Polymerase, New England Biolabs), purification of PCR products (QIAquick PCR Purification Kit, Qiagen), and Sanger sequencing (University of Wisconsin-Madison Biotechnology Center). One SNP in HPA3 (A→C in nucleotide 10 of the coding sequence causing a threonine 4 to proline change) in Y127 identified from the Illumina sequencing was not confirmed by Sanger sequencing. Further investigation determined that this mutation occurred during propagation.
of the strain for isolation of genomic DNA. Silent and intergenic mutations were not independently verified. All DNA sequencing reads have been deposited in the NCBI SRA under Bio-Project PRJNA279877.

**Cell culturing and phenotypic growth assays**

Aerobic tube and anaerobic flask growth and sugar consumption assays were performed as previously described [10] with some modifications. In the combined cell growth, proteomic and metabolomic studies, which generated data described in Figs 2–6 and S7–S10 Figs, yeast cells were grown in YPD media to log phase and then shifted into flasks containing 250 mL YPX media at a concentration of optical density at λ = 600 nm (OD<sub>600</sub>) = 0.3 for strains that could grow on xylene or OD<sub>600</sub> = 0.6 for strains that do not grow on xylene. For anaerobic experiments, cells were shifted into YPX media that was placed 16 h prior in an anaerobic chamber (Coy) containing 10% H<sub>2</sub>, 10% CO<sub>2</sub>, and 80% N<sub>2</sub> gases, and grown by stirring with a magnetic stir bar. Cell density, extracellular xylose and ethanol concentration measurements were taken at 0, 6.5, 8.5, 11, 13 and 17 h after inoculation for aerobic experiments, and 0, 8, 10, 14, 19, 20, and 32 h after inoculation for anaerobic experiments. Cells were harvested 14 h (for aerobic cultures) or 20 h (for anaerobic cultures) for proteomic (see below), metabolomic (see below), and dry cell weight analyses. Dry cell weight (DCW) measurements and anaerobic bioreactor fermentations in YPX + phosphate buffer, pH5.5 were performed as previously described [10]. For cell culture experiments to examine the respiration of various carbon substrates (Fig 6C and 6D), Y263 cells were grown to log phase in YPD media aerobically, and then shifted into flasks containing 50 mL fresh YPD, YPX or YP-Ethanol media and incubated at 30°C with shaking. After 6 h (for YPD cultures) or 10 h (for YPX or YP-Ethanol) of growth, 10 mL of culture was transferred to sterile test tubes and treated with 10 μL DMSO or 10 μL of 0.5 mg/mL Antimycin A (0.5 μg/mL final concentration, Sigma-Aldrich). Cell density (OD<sub>600</sub>) measurements were made with a Beckman DU720 spectrophotometer. Glucose, xylose, galactose, glycerol, acetate and ethanol concentrations for all experiments were determined by YSI 2700 Select instrument of by high performance liquid chromatography (HPLC) and refractive index detection (RID) [87].

**Specific consumption and ethanol production rate calculations**

Cell growth, specific xylose consumption and ethanol productivity rates were calculated with a rate estimation tool (S1 and S2 Appendices) using cell density (OD<sub>600</sub> or DCW), extracellular sugar and ethanol concentrations measured by HPLC-RID. The growth and substrate uptake or product secretion rates were determined by fitting the data to different linear equations using linear regression. The linear equations used to estimate growth and uptake rates, depended on whether data was from exponential growth, linear growth, or stationary (i.e., non-growth) phases. In the exponential (or linear) phase, the cell concentration increases exponentially (or linearly) with time, while in stationary phase the cell concentration remains constant. Mathematical details and instructions on using this rate-estimating tool can be found in S2 Appendix.

**Intracellular protein quantification**

After 14 or 20 h of culturing in YPX medium aerobically or anaerobically, respectively (see above), 25 mL of cell culture from each flask was transferred to 50 ml conical tubes, centrifuged at 10,000 RCF for 5 minutes at 4°C. Supernatants were decanted, cells were washed and centrifuged in TE buffer (10 mM Tris pH 7.0, 1 mM EDTA, Life Technologies) and cell pellets flash frozen in dry ice-ethanol for storage. Yeast cell pellets were suspended in 6M guanidine
hydrochloride (Sigma, St. Louis, MO) with 50 mM Tris pH 8.0 (Sigma, St. Louis, MO), boiled for 5 min, and methanol was added to a final concentration of 90% to lyse cells and precipitate protein. The precipitate was centrifuged at 10,000 RCF for 5 min, decanted, and air-dried. The protein pellet was resuspended in 8 M urea (Sigma, St. Louis, MO) with 100 mM Tris pH 8.0, 10 mM Tris (2-carboxyethyl) phosphine (Sigma, St. Louis, MO), and 40 mM chloroacetamide (Sigma, St. Louis, MO). The sample was diluted to 1.5 M urea with 50 mM Tris pH 8.0, and trypsin was added to a final ratio of 1:20 (enzyme to protein) followed by overnight incubation at ambient temperature. Tryptic peptides were desalted over Strata-X cartridges (Phenomenex, Torrance, CA). Desalted peptides were dried in a speed vac and resuspended in 0.2% formic acid. Peptides were quantified with the Pierce quantitative colorimetric peptide assay kit (Thermo Fisher Scientific, Rockford, IL). For each analysis, 2 μg of peptides were separated across a 30 cm, 75 μm internal diameter (i.d.) column packed with 1.7 μm BEH C18 particles (Waters, Milford, MA) housed in a capillary column heater set to 65°C. Mobile phase A was 0.2% formic acid and B was 0.2% formic acid, 70% ACN. Peptides were eluted with gradient of 5–50% B over 70 or 100 minutes for anaerobic and aerobic samples, respectively, followed by a 100% B wash and re-equilibration with 0% B [88]. Eluted peptides were analyzed on a Thermo Orbitrap Fusion Lumos (Thermo Fisher Scientific, San Jose, CA). Orbitrap survey scans were performed at 60,000 resolving power with an AGC of 106. The most intense precursors were isolated by the quadrupole with width 1 Da and AGC set to 104, and fragmented by higher energy collisional dissociation in the ion-routing multipole with normalized collision energy set to 30. Fragments were analyzed by turbo scan resolution ion-trap ms/ms. Only precursors with z = 2–8 were sampled, cycle time was set to < 2 s, and dynamic exclusion was 5 s. The maximum injection time for each ms/ms was 15 or 25 ms for anaerobic and aerobic samples, respectively. All analysis of the raw data was performed in the MaxQuant software suite version 1.5.2.8 [89, 90]. Default settings were used except, LFQ and matching between runs were enabled, ITMS match tolerance was set to 0.4 Da, and the min ratio count for quantitation was set to 1. Spectra were searched against a Saccharomyces cerevisiae Y22-3 protein database [91] and common contaminant database concatenated with the reverse sequences and filtered to 1% FDR at the peptide and protein level using the target-decoy approach using a reverse decoy database [92]. Raw data files for mass spectrometry proteomic data are available at https://chorusproject.org/pages/dashboard.html#/projects/all/1074/experiments (Project ID 1074). Significant differences in protein abundance were identified using edgeR on the protein-level counts, through pairwise strain comparisons [93], taking an FDR < 0.05 as significant. Functional enrichment was assessed using the FunSpec database [94]. Log2 fold-change calculations for protein abundances comparing mutant strains and the Y22-3MR parent strain grown in YPX under aerobic and anaerobic conditions are provided in S6 Appendix.

**Intracellular metabolite quantification**

For analysis of intracellular metabolites from yeast strains cultured in YPX media aerobically or anaerobically, cell samples were captured and harvested as described in [10] with minor changes. 20 mL of cell culture was applied to a filtration manifold unit (Hoefer FH 225V) outfitted with sterile 0.2 μm pore size nylon filters (Whatman), and the cells captured on the filters under vacuum. The filters were then immediately removed, placed in 15 mL conical tubes containing 4 mL ice-cold extraction buffer (acetonitrile-methanol-water, 40:40:20, 0.1% formic acid) and flash frozen. The concentrations of intracellular ribose-5-phosphate, ribulose-5-phosphate, dihydroxyacetone phosphate, glutathione, xylulose-5-phosphate, trehalose, xylose, xylulose, and xylitol were determined as previously described [10]. Quantifications of all other metabolites were performed as described elsewhere [87]. Log2 fold-change
calculations for metabolite abundances comparing mutant strains and the Y22-3^{MR} parent strain grown in YPX under aerobic and anaerobic conditions are provided in **S6 Appendix**.

**Supporting Information**

**S1 Fig.** Epistatic interactions between *hog1Δ* and *isu1Δ* mutations confer rapid aerobic xylose metabolism. The Y22-3^{MR} parent strain was engineered with various combinations of *isu1Δ*, *hog1Δ* and *gsh1Δ* (A, B) or *isu2Δ* and *hog1Δ* (C, D) mutations and cultured in YPX media aerobically. Extracellular xylose concentrations (A and C) and cell densities (B and D) from the cultures at the indicated times are plotted. Values displayed are averages and standard deviations from three independent biological experiments. The asterisks (*) denote statistical significance between the indicated strains and *isu1Δ* single mutant by paired Student's t-test, \( P < 0.05 \).

(TIF)

**S2 Fig.** Deletion of *IRA2* and *GRE3* enables aerobic to anaerobic xylose metabolism. Combinations of *gre3Δ*, *ira2Δ* and *sap190Δ* (A-B) or *gre3Δ* and *ira1Δ* mutations (C-D) were engineered in the Y127^{MR} and Y128^{MR} strains, which also contained aerobically evolved *hog1*, *isu1* and *gsh1* mutations. Engineered strains were then cultured in YPX media anaerobically, and extracellular xylose concentrations (A, C) and cell densities (B, D) were measured at the indicated times. Values plotted are averages and standard deviations of 2–3 independent biological replicates.

(TIF)

**S3 Fig.** Deletions of *ISU1*, *HOG1*, *GRE3* and *IRA2* are sufficient to increase xylose fermentation rates. Specific ethanol productivity rates in g of ethanol produced\( \cdot \)g of dry cell mass^{-1}\cdot h^{-1} (A) or g of ethanol produced\( \cdot \)OD\(_{600}\)^{-1}\cdot h^{-1} (B) from the indicated strains cultured in anaerobic YPX media were calculated from three independent biological replicates. Asterisks denote statistically significant differences (*; \( P < 0.05 \), **; \( P < 0.063 \)) between indicated strains by paired Student's t-test.

(TIF)

**S4 Fig.** Deletions of *ISU1*, *HOG1*, *GRE3* and *IRA2* are sufficient to increase cell growth and xylose consumption rates in anaerobic bioreactors. Indicated strains were cultured in YPX media in bioreactors continually sparged with 100% \( \text{N}_2 \). Specific growth and xylose consumption rates in OD\(_{600}\)^{-1}\cdot hr^{-1} (A) and g of xylose consumed\( \cdot \)OD\(_{600}\)^{-1}\cdot h^{-1} (B) from the indicated strains cultured in YPX media. Graphed average values and standard deviations were calculated from two independent biological replicates.

(TIF)

**S5 Fig.** Deletions of *ISU1*, *HOG1*, *GRE3* and *IRA2* are sufficient for anaerobic xylose metabolism in other strain backgrounds. Indicated strains were cultured in YPX media under anaerobic conditions. Average cell growth (A), specific xylose consumption (B) and ethanol productivity (C) rates in cell mass (in OD\(_{600}\)^{-1}\cdot h^{-1}, g xylose, consumed or ethanol produced\( \cdot \)L^{-1}\cdot h^{-1}\cdot cell mass (in OD\(_{600}\)^{-1}), respectively, were calculated from three independent replicates and plotted. Asterisks denote statistically significant differences (*; \( P < 0.05 \), **; \( P < 0.08 \)) between indicated strains by paired Student's t-test.

(TIF)

**S6 Fig.** Deletions of *HOG1* and *ISU1* have different effects on the metabolism of other carbon substrates. The schematic diagram in (A) displays the routes of catabolism for the indicated carbon substrates through central metabolism. Dashed arrows indicate that multiple
biochemical reactions are involved before the substrate enters central metabolism. Bar graphs display cell growth and specific consumption rates for galactose (B-C), ethanol (D-E) aerobically, and galactose anaerobically (F-G) for the indicated strains. Reported values are averages and standard deviations from biological triplicate experiments, and in g substrate consumed or ethanol produced • L⁻¹ • h⁻¹ • cell mass (in OD₆₀₀)⁻¹. Asterisks denote statistically significant differences (P < 0.05) by Student’s t-test.

S7 Fig. Global proteomic analysis identified overlapping functional groups with increased or decreased expression in xylose metabolizing strains. Venn diagrams showing overlap in proteins that increased (left) or decreased (right) in expression level for the indicated xylose metabolizing strains relative to control strains under aerobic (A) or anaerobic (B) conditions with an FDR of 0.05.

S8 Fig. Strains with mutations in IRA2 display altered levels of trehalose biosynthesis enzymes and intracellular trehalose. Schematic diagram trehalose biosynthesis pathways are displayed (A). Heat maps display average log₂ fold differences in trehalose biosynthesis enzymes for the indicated strains relative to Y22-3³MR under aerobic (B) or anaerobic (C) YPX conditions. Bar graphs display average intracellular trehalose concentrations in µm/g of DCW under aerobic (D) or anaerobic (E) conditions. All average values and standard deviations were calculated from three independent biological replicates.

S9 Fig. TCA Cycle metabolite profiles do not correlate with enzyme profiles in xylose consuming strains. Schematic diagram of the TCA Cycle pathway is displayed (A). Heat maps display average Log₂ fold differences in metabolite (B-C) and protein (D-E) levels for the indicated strains relative to Y22-3³MR under aerobic (B and D) or anaerobic (C and E) YPX conditions. White boxes indicate strains from which no metabolite was detected. Average Log₂ fold differences were calculated from three independent biological replicates. 2-OG, 2-oxoglutarate.

S10 Fig. The expression profile of glucose-repressed proteins in anaerobic conditions is distinct from that in aerobic conditions. Engineered and evolved strains were cultured in aerobic YPX media and analyzed for intracellular protein and metabolite concentrations. Average Log₂ intracellular concentrations of mitochondrial translation and respiration proteins (A) or hexose transporters and glucose-repressed proteins (B) from mutant strains relative to the Y22-3³MR parent are shown. White boxes indicate strains for which no corresponding peptides were detected. Relative protein concentrations were calculated from three independent biological replicates are reported.

S1 Table. S. cerevisiae strains and their genotypes used in this study.

S1 Appendix. Batch Culture Rate Estimation Tool version 1.0 By Mingyuan Tian, Jennifer Reed Lab, Chemical & Biological Engineering, University of Wisconsin-Madison.

S2 Appendix. User Manual for Batch Culture Rate Estimation Tool.
S3 Appendix. Comparing Protein Overlap—Increasing Protein in YPX aerobic, S7A Fig. (XLSX)

S4 Appendix. EdgeR Log2-fold changes and FDRs for pair-wise protein abundance comparisons between yeast strains grown in YPX aerobic. (XLSX)

S5 Appendix. EdgeR Log2-fold changes and FDRs for pair-wise protein abundance comparisons between yeast strains grown in YPX anaerobic. (XLSX)

S6 Appendix. Log2 normalized values for proteomic and metabolomic data. (XLSX)

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Validation: TKS APG RL.
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Writing – original draft: TKS APG RL.
Writing – review & editing: TKS LSP ASH CTH APG RL.

References


**S1 Fig.** Epistatic interactions between *hog1Δ* and *isu1Δ* mutations confer rapid aerobic xylose metabolism.

The Y22-3^{MR} parent strain was engineered with various combinations of *isu1Δ, hog1Δ* and *gsh1Δ* (A, B) or *isu2Δ* and *hog1Δ* (C, D) mutations and cultured in YPX media aerobically. Extracellular xylose concentrations (A and C) and cell densities (B and D) from the cultures at the indicated times are plotted. Values displayed are averages and standard deviations from three independent biological experiments. The asterisks (*) denote statistical significance between the indicated strains and *isu1Δ* single mutant by paired Student’s t-test, *P* < 0.05.

doi:10.1371/journal.pgen.1006372.s001 (TIF)

**S2 Fig.** Deletion of *IRA2* and *GRE3* enables aerobic to anaerobic xylose metabolism.

Combinations of *gre3Δ,ira2Δ* and *sap190Δ* (A-B) or *gre3Δ* and *ira1Δ* mutations (C-D) were engineered in the Y127^{MR} and Y128^{MR} strains, which also contained aerobically evolved *hog1,sis1* and *gsh1* mutations. Engineered strains were then cultured in YPX media anaerobically, and extracellular xylose concentrations (A, C) and cell densities (B, D) were measured at the indicated times. Values plotted are averages and standard deviations of 2–3 independent biological replicates.

doi:10.1371/journal.pgen.1006372.s002 (TIF)

**S3 Fig.** Deletions of *ISU1, HOG1, GRE3* and *IRA2* are sufficient to increase xylose fermentation rates.

Specific ethanol productivity rates in g of ethanol produced•g of dry cell mass^{-1}•h^{-1} (A) or g of ethanol produced•OD_{600}{^{-1}}•h^{-1} (B) from the indicated strains cultured in anaerobic YPX media were calculated from three independent biological replicates. Asterisks denote statistically significant differences (*; *P* < 0.05, **; *P* < 0.063) between indicated strains by paired Student’s t-test.

doi:10.1371/journal.pgen.1006372.s003 (TIF)

**S4 Fig.** Deletions of *ISU1, HOG1, GRE3* and *IRA2* are sufficient to increase cell growth and xylose consumption rates in anaerobic bioreactors.

Indicated strains were cultured in YPX media in bioreactors continually sparged with 100% N_{2}. Specific growth and xylose consumption rates in OD_{600}•hr^{-1} (A) and g of xylose consumed•OD_{600}^{-1}•h^{-1} (B) from the indicated strains cultured in YPX media. Graphed average values and standard deviations were calculated from two independent biological replicates.

doi:10.1371/journal.pgen.1006372.s004 (TIF)

**S5 Fig.** Deletions of *ISU1, HOG1, GRE3* and *IRA2* are sufficient for anaerobic xylose metabolism in other strain backgrounds.
Indicated strains were cultured in YPX media under anaerobic conditions. Average cell growth (A), specific xylose consumption (B) and ethanol productivity (C) rates in cell mass (in OD_{600}•h^{-1}, g xylose, consumed or ethanol produced•L^{-1}•h^{-1}•cell mass (in OD_{600}^{-1}), respectively, were calculated from three independent replicates and plotted. Asterisks denote statistically significant differences (*; p < 0.05, **; p < 0.08) between indicated strains by paired Student’s t-test.

doi:10.1371/journal.pgen.1006372.s005

(S6 Fig. Deletions of HOG1 and ISU1 have different effects on the metabolism of other carbon substrates.

The schematic diagram in (A) displays the routes of catabolism for the indicated carbon substrates through central metabolism. Dashed arrows indicate that multiple biochemical reactions are involved before the substrate enters central metabolism. Bar graphs display cell growth and specific consumption rates for galactose (B-C), ethanol (D-E) aerobically, and galactose anaerobically (F-G) for the indicated strains. Reported values are averages and standard deviations from biological triplicate experiments, and in g substrate consumed or ethanol produced•L^{-1}•h^{-1}•cell mass (in OD_{600}^{-1}). Asterisks denote statistically significant differences (P < 0.05) by Student’s t-test.

doi:10.1371/journal.pgen.1006372.s006

(S7 Fig. Global proteomic analysis identified overlapping functional groups with increased or decreased expression in xylose metabolizing strains.

Venn diagrams showing overlap in proteins that increased (left) or decreased (right) in expression level for the indicated xylose metabolizing strains relative to control strains under aerobic (A) or anaerobic (B) conditions with an FDR of 0.05.

doi:10.1371/journal.pgen.1006372.s007

(S8 Fig. Strains with mutations in IRA2 display altered levels of trehalose biosynthesis enzymes and intracellular trehalose.

Schematic diagram trehalose biosynthesis pathways are displayed (A). Heat maps display average log2 fold differences in trehalose biosynthesis enzymes for the indicated strains relative to Y22-3^MR under aerobic (B) or anaerobic (C) YPX conditions. Bar graphs display average intracellular trehalose concentrations in µm/g of DCW under aerobic (D) or anaerobic (E) conditions. All average values and standard deviations were calculated from three independent biological replicates.

doi:10.1371/journal.pgen.1006372.s008

(S9 Fig. TCA Cycle metabolite profiles do not correlate with enzyme profiles in xylose consuming strains.
Schematic diagram of the TCA Cycle pathway is displayed (A). Heat maps display average Log$_2$ fold differences in metabolite (B-C) and protein (D-E) levels for the indicated strains relative to Y22-3$^{MR}$ under aerobic (B and D) or anaerobic (C and E) YPX conditions. White boxes indicate strains from which no metabolite was detected. Average Log$_2$ fold differences were calculated from three independent biological replicates. 2-OG, 2-oxoglutarate. doi:10.1371/journal.pgen.1006372.s009 (TIF)

**S10 Fig.** The expression profile of glucose-repressed proteins in anaerobic conditions is distinct from that in aerobic conditions.

Engineered and evolved strains were cultured in aerobic YPX media and analyzed for intracellular protein and metabolite concentrations. Average Log$_2$ intracellular concentrations of mitochondrial translation and respiration proteins (A) or hexose transporters and glucose-repressed proteins (B) from mutant strains relative to the Y22-3$^{MR}$ parent are shown. White boxes indicate strains for which no corresponding peptides were detected. Relative protein concentrations were calculated from three independent biological replicates are reported. doi:10.1371/journal.pgen.1006372.s010 (TIF)
## S1 Table. *S. cerevisiae* strains and their genotypes used in this study.

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This excel worksheet is used to calculate the growth rates and uptake (or secretion) rates in exponential growth, linear growth, and/or stationary (i.e., no growth) phases from concentration data measured in batch culture experiments. The input data are tables of time and OD and time and substrate concentrations.

How to use it?

Be sure to turn on automatic calculation in Excel (this ensures that the cells are updated after you enter your data—you should see the results change after copying in your data):

On a PC with Excel 2010 and 2013: Go to File > Options > Formulas > Workbook Calculation > Automatic.

If the values in the yellow “results” boxes do not update automatically, their values can be updated manually by double-clicking on the corresponding cells and then pressing enter (without changing any of the equations).

The LINEST function from Excel was used to determine the slopes and intercepts (and their standard deviations) for a series of linear least squares regressions (described below).

1. In the “OD vs time” worksheet:

   1.1 Paste your time and OD data for the complete experiment into the blue table on the lower left. Make sure to expand the blue table so that it includes all of the data by dragging the lower right corner of the blue table. Evaluate the resulting graphs and decide which time points correspond to exponential growth, linear growth, and stationary (i.e. no growth) phases. Exponential growth should correspond to points that are linear on the ln(OD) versus time graph. Linear growth should correspond to points that are linear on the OD versus time graph. Stationary growth should correspond to points that have an almost constant OD over a period of time.

2. In the “exponential growth phase” worksheet:

   2.1 Paste your time and OD data corresponding to the exponential growth phase under the orange columns labeled ‘time(h)’ and ‘OD’. Since the equations being fit to the data assume the exponential phase starts at time $t = 0$, the times need to be normalized by subtracting the initial time ($t_0$) from all the times. Similarly, the OD data needs to be transformed by taking the natural log of the OD measurements. To transform the data into $t - t_0$ and $\ln(OD)$ drag the autofill symbol in the blue table immediately to the right of the inputted data. (See Figure 1)
Figure 1: Illustration for dragging the autofill symbol. Before dragging (Left). After dragging (Right).

2.2 Paste your OD and substrate concentration data corresponding to the exponential growth phase under the orange columns labeled ‘OD’ and ‘Substrate Concentration (g/L)’. Since the equations being fit to the data use the change in OD from the start of the exponential phase, the OD needs to be normalized by subtracting the initial OD \(OD(t_0)\) from all the ODs. To transform the data into \(OD(t) – OD(t_0)\) and Substrate Concentration drag the autofill symbol in the blue table immediately to the right of the inputted data.

2.3 After updating the values in these two blue tables, the estimated growth and substrate uptake rates can be found in the yellow cells along with their standard deviations. Their corresponding units are reported assuming time was measured in hours, biomass was measured as OD units, and substrate concentration was measured as g/L. To make sure the estimates seem reasonable the following should be checked:

- The estimated initial OD and substrate concentrations (below the yellow boxes) are similar to the measured initial concentrations in the orange tables.
- Both graphs show good linear relationships with the normalized data (\(R^2\) close to 1).

3. In the “linear growth phase” worksheet:

3.1 Paste your time and OD data corresponding to linear growth phase under the orange columns labeled ‘time(h)’ and ‘OD’. Since the equations being fit to the data assume the linear phase starts at time \(t = 0\), the times need to be normalized by subtracting the initial time \((t_0)\) from all the times. To transform the data into \(t – t_0\) and OD drag the autofill symbol in the blue table immediately to the right of the inputted data.

3.2 Paste your time and substrate concentration data corresponding to exponential growth phase under the orange columns labeled ‘time’ and ‘Substrate Concentration (g/L)’. To fit the data to the linear equation the data needs to be transformed. To transform the data into \(\frac{\mu}{2} \cdot (t – t_0)^2 + X_0 \cdot (t – t_0)\) and Substrate Concentration drag the autofill symbol in the blue table immediately to the right of the inputted data. Here, \(\mu\) is the best estimate for the linear growth rate and \(X_0\) is the best estimate for the initial biomass concentration (i.e., OD), which are both found by fitting the data inputted in step 3.1.

3.3 After updating the values in these two blue tables, the estimated growth and substrate uptake rates can be found in the yellow cells along with their standard deviations. Their corresponding units are reported assuming time was measured in hours, biomass was measured as OD units, and substrate concentration was measured as g/L. Note: the growth rate units are different in this worksheet than the other worksheets. To make sure the estimates seem reasonable the following should be checked:

- The estimated initial OD and substrate concentrations (below the yellow boxes) are similar to the measured initial concentrations in the orange tables.
- Both graphs show good linear relationships with the normalized data (\(R^2\) close to 1).

4. In the “stationary phase” worksheet:
4.1 Paste your **time** and **OD** data corresponding to stationary growth phase under the orange columns labeled ‘time’ and ‘OD’. Since the equations being fit to the data assume the linear phase starts at time $t = 0$, the times need to be normalized by subtracting the initial time ($t_0$) from all the times. To transform the data into $t - t_0$ and OD drag the autofill symbol in the blue table immediately to the right of the inputted data.

4.2 Paste your **time** and **substrate concentration** data corresponding to exponential growth phase under the orange columns labeled ‘time’ and ‘Substrate Concentration (g/L)’. Since the equations being fit to the data assume the linear phase starts at time $t = 0$, the times need to be normalized by subtracting the initial time ($t_0$) from all the times. To transform the data into $t - t_0$ and Substrate Concentration drag the autofill symbol in the blue table immediately to the right of the inputted data.

4.3 After updating the values in these two blue tables, the estimated substrate uptake rates can be found in the yellow cells along with its standard deviation. Their corresponding units are reported assuming time was measured in hours, biomass was measured as OD units, and substrate concentration was measured as g/L. To make sure the estimates seem reasonable the following should be checked:

- The estimated initial OD and substrate concentrations (below the yellow boxes) are similar to the measured initial concentrations in the orange tables.
- The green graph on the left shows a relatively constant OD over time.
- The grey graph on the right shows a good linear relationship with the normalized data ($R^2$ close to 1).
Equations used to Derive Linear Relationships Used to Estimate Growth or Uptake Rates:

The equations and derivations below describe how cell concentrations and substrate concentrations change during different phases of growth in a constant volume batch reactor.

\( X = \) cell concentration (units of OD)
\( X_0 = \) initial cell concentration at the beginning of the phase (units of OD)
\( t = \) time
\( t_0 = \) time the phase starts (normally corresponds to the first time point within a growth phase)
\( \mu = \) growth rate with units of 1/h or OD/h for exponential and linear growth, respectively.
\( S = \) substrate concentration (g/L)
\( S_0 = \) initial substrate concentration at the beginning of the phase
\( q = \) substrate consumption rate (g/L/OD/h)

**Exponential growth phase equations:**

The derivative for the change in biomass concentration during exponential growth in a batch reactor is given by Eq. 1 [1]:

\[
\frac{dX}{dt} = \mu X
\]  
(Eq. 1)

By integrating Eq. 1, a linear relationship can be derived (Eq. 2) so that doing a linear least squares regression between \( \ln X \) and \((t - t_0)\) will yield estimates for \( \mu \) (the slope) and \( \ln X_0 \) (the intercept).

\[
\ln X = \ln X_0 + \mu (t - t_0)
\]  
(Eq. 2)

The derivative for the change in substrate concentration in a batch reactor is given by Eq. 3 [1]:

\[
\frac{dS}{dt} = -qX
\]  
(Eq. 3)

By integrating Eq. 3, a linear relationship can be derived (Eq. 4) so that doing a linear least squares regression between \( S \) and \((X - X_0)\) will yield estimates for \( q \) (where \( q = -slope \cdot \mu \)) and \( S_0 \) (the intercept). The standard deviations for \( \mu \) and the slope were propagated to find the standard deviation for \( q \).

\[
S = S_0 - q \left( \frac{X - X_0}{\mu} \right)
\]  
(Eq. 4)

**Linear growth phase equations:**

The derivative for the change in biomass concentration during linear growth in a batch reactor is given by Eq. 5:

\[
\frac{dX}{dt} = \mu
\]  
(Eq. 5)

By integrating Eq. 5, a linear relationship can be derived (Eq. 6) so that doing a linear least squares regression between \( X \) and \((t - t_0)\) will yield estimates for \( \mu \) (the slope) and \( X_0 \) (the intercept).
The derivative for the change in substrate concentration in a batch reactor is given by Eq. 7:

$$\frac{ds}{dt} = -qX$$  \hspace{1cm} (Eq. 7)

By integrating Eq. 7, a linear relationship can be derived (Eq. 8) so that doing a linear least squares regression between $S$ and $\frac{\mu}{2} (t - t_0)^2 + X_0(t - t_0)$ will yield estimates for $q$ (where $q = -\text{slope}$) and $S_0$ (the intercept).

$$S = S_0 - q\left[\frac{\mu}{2} (t - t_0)^2 + X_0(t - t_0)\right]$$  \hspace{1cm} (Eq. 8)

### Stationary phase equations:

The derivative for the change in biomass concentration during stationary phase in a batch reactor is given by Eq. 9:

$$\frac{dx}{dt} = 0$$  \hspace{1cm} (Eq. 9)

By integrating Eq. 9, a linear relationship can be derived showing $X$ is a constant and is independent of time. For this phase, the average $X$ in that phase is represented as $\bar{X}$.

The derivative for the change in substrate concentration in a batch reactor is given by Eq. 10:

$$\frac{ds}{dt} = -qX = -q\bar{X}$$  \hspace{1cm} (Eq. 10)

By integrating Eq. 10, a linear relationship can be derived (Eq. 11) so that doing a linear least squares regression between $S$ and $(t - t_0)$ will yield estimates for $q$ (where $q = -\text{slope} \cdot \bar{X}$) and $S_0$ (the intercept). The standard deviations for $\bar{X}$ and the slope were propagated to find the standard deviation for $q$.

$$S = S_0 - q\bar{X}(t - t_0)$$  \hspace{1cm} (Eq. 11)

### References:

CORRECTION

Correction: Directed Evolution Reveals Unexpected Epistatic Interactions That Alter Metabolic Regulation and Enable Anaerobic Xylose Use by Saccharomyces cerevisiae

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Authorship

Dr. Jeff S. Piotrowski should be included in the author byline instead of the Acknowledgments. He should be listed as the seventeenth author, and his affiliation is: DOE Great Lakes Bioenergy Research Center, University of Wisconsin-Madison, Madison, Wisconsin, United States of America. The contribution of this author is as follows: Investigation.

Competing Interests

The competing interests statement is incorrect. The statement should read: I have read the journal's policy and the authors of this manuscript have the following competing interests: The Wisconsin Alumni Research Foundation has a provisional patent application entitled "Recombinant yeast having enhanced xylose fermentation capabilities and methods of use". TKS and JSP are inventors. MTr, LSP, ASH, KSM, AJH, MS, SJM, IMO, RJB, RAN, MAM, QD, AL, DX, MTi, JLR, YZ, JJC, CTH, APG, and RL have declared that no competing interests exist.

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